

# Conversion of CH<sub>4</sub> and CO<sub>2</sub> to value-added products

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**Abstract:** This study investigates the decomposition of CH<sub>4</sub> and CO<sub>2</sub> using a 30 kW triple thermal plasma system, producing hydrogen and high-value solid carbon. At the lowest CH<sub>4</sub> flow rate, CH<sub>4</sub> and CO<sub>2</sub> conversion rates were highest at 98% and 71%, respectively, graphene-like carbon synthesized. However, hydrogen selectivity was highest at 82% under the highest CH<sub>4</sub> flow rate.

## 1. Introduction

CO<sub>2</sub> and CH<sub>4</sub> are major greenhouse gases contributing to climate change. This study uses thermal plasma to convert CH<sub>4</sub> and CO<sub>2</sub> into H<sub>2</sub> and solid carbon[1]. Hydrogen offers zero-emission energy potential, while solid carbon materials like carbon black and graphene have industrial applications. This approach simultaneously reduces greenhouse gases and produces valuable materials[2].

## 2. Methods

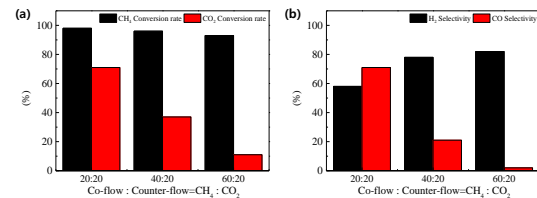
In this study, a 30 kW triple thermal plasma system with three DC torches, a dual injection nozzle, a reactor, and a filter were used. In particular, we designed the injection nozzle separately to control the characteristics of solid carbon. CH<sub>4</sub> was injected through the co-flow injection nozzle. And CO<sub>2</sub> was injected through the counter-flow injection nozzle. The CO<sub>2</sub> flow rate was fixed at 20 L/min, while CH<sub>4</sub> flow rates ranged from 20 to 60 L/min. Gas Chromatography (GC) measured product gas ratios, determining CH<sub>4</sub> and CO<sub>2</sub> conversion rates, H<sub>2</sub> selectivity, and CO selectivity. Solid carbon produced during the process was analyzed using Field Emission Transmission Electron Microscopy to examine its morphology.

## 3. Results and Discussion

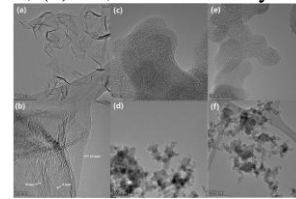
Based on Gas Chromatography (GC) data, the CH<sub>4</sub> and CO<sub>2</sub> conversion rates, as well as H<sub>2</sub> and CO selectivity, were analyzed. As the methane flow rate increased threefold from 20 to 60 L/min, the CH<sub>4</sub> conversion rate remained above 90%. This suggests that the energy density of the thermal plasma was sufficient for CH<sub>4</sub> conversion at 60 L/min of CH<sub>4</sub> flow rate. However, although the CO<sub>2</sub> flow rate was fixed, its conversion decreased by approximately 60%, reaching 11% as the CH<sub>4</sub> flow rate increased. The high CH<sub>4</sub> conversion rate indicates that the energy density of thermal plasma was sufficient for CO<sub>2</sub> conversion. However, the low CO<sub>2</sub> conversion is presumed to be due to the secondary reactions between CO and C at the reactor of the lower part, leading to the formation of CO<sub>2</sub>. The H<sub>2</sub> selectivity increased with the rise in CH<sub>4</sub> flow rate, exhibiting a trend opposite that of CO selectivity. It is presumed that the lower CO selectivity can be attributed to the same reason as the lower CO<sub>2</sub> conversion rate.

Additionally, the characteristics of the synthesized solid carbon varied with the CH<sub>4</sub> flow rate. A multilayered,

sheet-like carbon structure was formed at the lowest flow rate. In contrast, solid carbon with a vortex-layered structure characteristic of carbon black was synthesized at the highest flow rate.



**Fig. 1.** According to CH<sub>4</sub> flow rate (a) CH<sub>4</sub>, CO<sub>2</sub> conversion rate, (b) H<sub>2</sub>, CO selectivity.



**Fig. 2.** TEM image of synthesized solid carbon according to CH<sub>4</sub> flow rate: CO<sub>2</sub> flow rate (a,b) 20:20, (c,d) 40:20, (e,f) 60:20.

## 4. Conclusion

This study demonstrated the simultaneous conversion of CH<sub>4</sub> and CO<sub>2</sub> using a triple thermal plasma system, producing hydrogen and high-value solid carbon. Hydrogen selectivity increased with higher CH<sub>4</sub> flow rates, while CO<sub>2</sub> conversion and carbon monoxide selectivity decreased. Solid carbon with varying morphologies, including vortex-layered carbon black, was synthesized. Future work will aim to identify optimal conditions for maximizing both hydrogen production and solid carbon synthesis simultaneously.

## Acknowledgement

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## References

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